
EXPERIMENTAL QUANTITATIVE EVALUATION OF THERMAL PERFORMANCE IN REFRIGERATED DISPLAY CABINETS WITH VARIATION OF AIR CURTAIN THICKNESS AND POROSITY OF THE BACK PANEL

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ABSTRACT

Open multideck display cabinets are widely used to expose perishable products in supermarkets and convenience stores. This paper reports the results of experimental tests performed according to ISO23953 in a open multideck refrigerated display cabinet to assess the impact on the thermal performance by varying the width of the discharge air grille and the perforation density of the back panel. The experimental laboratory tests were conducted for climate class n.º 3 (25° C and 60%). The results evaluation shows that the perforation density of the back panel and the width of discharge air grille alter significantly the thermal entrainment factor and the energy consumption of the equipment. The best performance configuration showed a 10% reduction of the cooling load. The analysis of the results provides valuable information for the development of these equipments.

1. INTRODUCTION

Since ancient times, man has the need and the will of obtaining cooling ways that make the temperature of foods products to reach a value below the environmental temperature in order to preserve them for longer periods of time. The perishable food products, from production to the final consumer, are preserved and channelled through the system named as cold chain. According to Rigot (1991), the cold chain can be described by five main links: Cold in the production stage; Cold during storage, Refrigerated transportation; Cold in the distribution stage; Home cooling. The fourth link in the cold chain, which is the subject of this paper, is commonly referred as commercial refrigeration by being placed at the trade level. ASHRAE (2010) indicates that the percentage of energy consumed in a typical supermarket due to the refrigeration systems reaches 50%. This energy is consumed by compressors, refrigerated display cabinets, walk-ins and condensers. Among the refrigerated display cabinets installed in a supermarket, which consumes more energy are of the vertical and open type. According to Faramarzi (1999), ASHRAE (2010) and Gaspar *et al.* (2011), the thermal load due to ambient air infiltration to a vertical open refrigerated display cabinet (ORDC) corresponds respectively to 67% - 77%, 73.5% and 78% - 81% of the total thermal load. This condition results from the low efficiency of the curtain air which forms a physical barrier between the internal and external environments of the equipment.

The work developed by various researchers has focused, for this type of equipment, in qualifying and quantifying the perceptible thermo-physical properties of the jet that provides a cold air curtain. Hayes & Stoecker (1969) developed a correlation that describes the ability of the air curtain to provide a proper separation between environments. The correlation is given by a dimensionless parameter named as deflection modulus, D_m , which is the ratio between the air curtain momentum and the modulus of the transverse forces caused by temperature difference between the contiguous environments. Faramarzi (1999) determined the relative weight of the total cooling load components for ORDC, composed by the loads from infiltration, radiation, conduction, product pull-down cooling, devices (lights and fans), defrost and anti-sweat heaters, and product respiration. According to EN-ISO 23953 (2005), the total thermal cooling load can be determined by eq. (1).

$$\dot{Q}_{tot} = \dot{m}_{ref} \cdot \Delta i \quad (1)$$

Chen *et al.* (2005, 2009, 2011) developed studies using Computational Fluid Dynamics (CFD) codes to evaluate the thermo-physical parameters of the air curtain in ORDC. The performance of air curtain was evaluated by the following dimensionless numbers/parameters: Reynolds number, Grashof number, Richardson number and dimensionless temperature, given by eq. (2) to eq. (5) respectively, for different aspect ratios (height/width) of the air curtain.

$$Re = \left(\frac{u \cdot b}{\nu} \right)_{DAG} \quad (2)$$

$$Gr = \frac{g \xi (T_{amb} - T_{DAG}) H^3}{\nu_{DAG}^2} \quad (3)$$

$$Ri = \frac{Gr}{Re^2} \quad (4)$$

$$X_j = \frac{T_{RAG} - T_{DAG}}{T_{Amb} - T_{DAG}} \quad (5)$$

The results provided the following conclusions: There is a range of values of Reynolds number quantifying the flow that can be reduced by reducing the height/width ratio of the air jet for optimal thermal insulation developed by the cold air curtain jet; As the Grashof number provides the fluctuation proportion of the buoyancy force that acts on a viscous fluid in situations involving heat transfer by natural convection while the Richardson number provides the information on the influence of natural convection in relation to forced convection, it is possible to use them for describe the flow. Thus it can be stated that air curtains with small height/width ratio provide a good thermal performance. Navaz *et al.* (2005) developed further studies using Digital Particle Image Velocimetry (DPIV), focusing mainly in studying the effectiveness of the curtain and maintaining the temperature of food products to a predetermined value. The results evaluation indicates that the Reynolds number has direct effect on the ambient air entrainment into the refrigerated equipment due to its role in the turbulence development. According to Navaz *et al.* (2005), the best range of values for the Reynolds number in the discharge air grille (DAG) is about 3200-3400. In that study, the authors defined the Thermal Entrainment Factor, *TEF*, to quantify the thermal entrainment of the air curtain with the ambient air, varying $0 < TEF < 1$.

The analysis to the correlation shows that as closer to 0 is *TEF*, lower is the thermal entrainment with the ambient air. The correlation described by Navaz *et al.* (2005) does not take into account the air flow through the perforated back panel (PBP). Yu *et al.* (2009) developed the *TEF* equation considering this air flow. The new correlation is given by eq. (6) to eq. (8) including the dimensionless temperature given by eq. (5).

$$TEF = (1 - \beta)X_j - \beta X_j X_{PBP} \quad (6)$$

$$\beta = \frac{\dot{m}_{PBP}}{\dot{m}_{PBP} + \dot{m}_{DAG}} \quad (7)$$

$$X_{PBP} = \frac{T_{PBP} - T_{DAG}}{T_{Amb} - T_{DAG}} \quad (8)$$

The results obtained by Yu *et al.* (2009) show a good approximation for *TEF* and temperature value at the return air grille (RAG) with deviations of 0.9% and 0.1 °C respectively. These deviations indicate that the correlation has a good approximation at the engineering level and can be applied in the design of vertical ORDC. Gaspar *et al.* (2009, 2010, 2011) evaluated the stability of the air curtain for climatic classes n.º 1, n.º 2 and n.º 3 according to EN-ISO 23953 (2005) and other classes beyond the standard. The evaluation was made by experimental testing and numerically using CFD models. The results showed that the ORDC performance strongly depends on the ambient air conditions such as temperature, humidity, velocity and direction of ambient air flow in relation to the ORDC's frontal opening. These authors showed that (1) the cooling load increases with the air temperature and relative humidity of the external environment, (2) the increase of the ambient air velocity increases more significantly the power consumption of the ORDC than the airflow direction change from parallel to perpendicular in relation the frontal opening of the ORDC, (3)

the magnitude of deflection modulus D_m related with minimum momentum required to maintain a stable curtain of air is between 0.12 and 0.25; (4) the cooling load due to air infiltration is 78% - 81%, which is range closer to the value obtained by Faramarzi (1999) which is of 73.5%, and (5) TEF is not constant along the equipment length for parallel air flow. Furthermore, the TEF value increases when the ambient air flow goes from parallel to perpendicular, being the worst case for $\theta_{amb} = 45^\circ$. In the case study, $TEF = 0.25, 0.32, 0.3$ for $\theta_{amb} = 0^\circ, 45^\circ, 90^\circ$ respectively.

Laguerre *et al.* (2012) developed a simplified analytical model based on heat transfer equations to determine the values of air and product temperatures at various locations of an ORDC. The heat gain by radiation is more significant for products located on the front (top and bottom) and the heat gain by air infiltration is more significant for the products located in the rear (front and rear). Cao *et al.* (2010, 2011) developed a new strategy for conception and optimization in the air curtains design for vertical ORDC. The strategy is based on the heat transfer model between two fluids (two-fluid of cooling loss - CLTF) developed based on a Support Vector Machine (SVM) algorithm.

This paper aims to contribute to studies on the thermal performance of ORDC, showing and evaluating the experimental results of the relation between the porosity of PBP and the GDA width on the overall performance of the ORDC.

2. EXPERIMENTAL STUDY

2.1. Experimental apparatus

The vertical ORDC provided by Eletrofrío Refrigeration LTDA - Brazil has $2.5 \times 1.1 \times 2.1 \text{ m}^3$. It comprises (1) an insulating body (IB) surrounding all the equipment; (2) tube and fins heat exchanger (HX); (3) discharge air grille (DAG); (4) return air grille (RAG); (5) perforated back panel (PBP) and shelves (SH) as shown in Figure 1. The temperature of the refrigerated compartment is provided by the cold air mass flow that exits DAG and PBP and returns to RAG to be cooled again in the HX. The air flow exiting DAG forms an air curtain which protects the inner refrigerated compartment. Note that this equipment has a primary air curtain (PAC) and a secondary air curtain (SAC) in order to promote a more effective aerothermodynamics sealing.

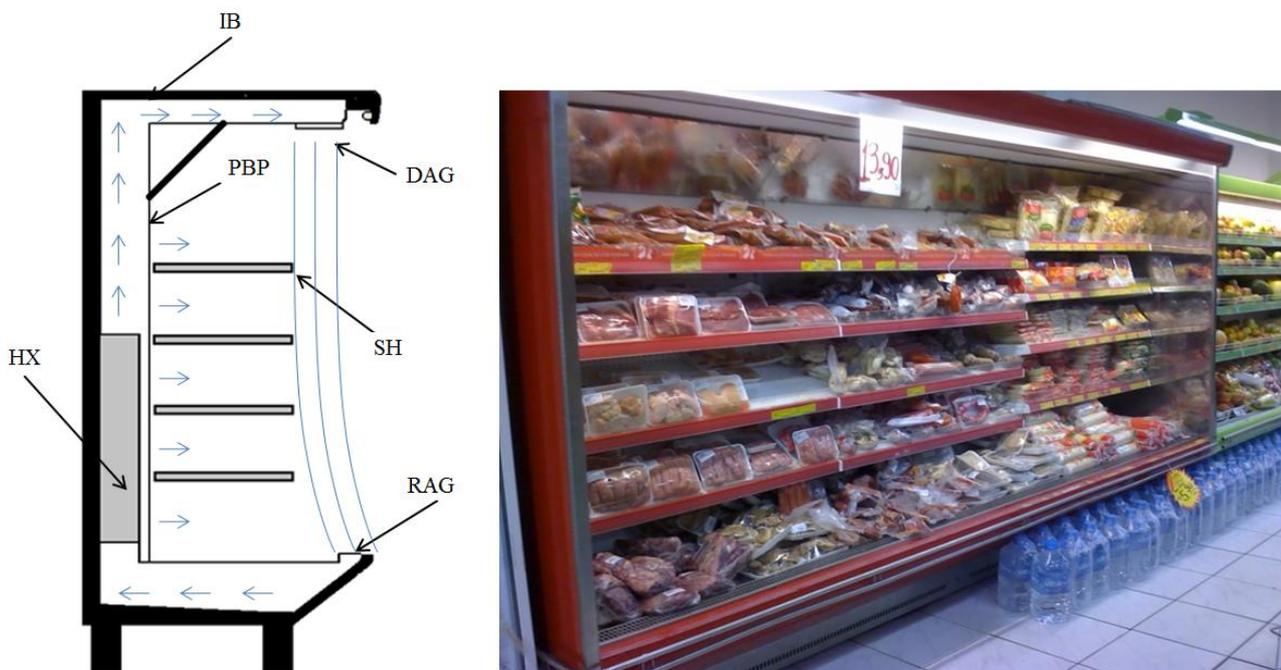


Figure 1. Vertical open refrigerated display cabinet.

The device has four fans with 53 W each to supply a flow rate of $0.4 \text{ m}^3 \cdot \text{s}^{-1}$ to DAG and PBP. The air, before reaching the DAG, passes through an evaporator with dimensions $2.20 \times 0.13 \times 0.35 \text{ m}^3$ constituted by 222 fins and three rows of tubes in the air flow direction and 8 rows of tubes perpendicular to it. The DAG has a total width, b , of 140 mm, which is equally distributed to form the PAC ($b_{PAC} = 70 \text{ mm}$) and SAC ($b_{SAC} = 70 \text{ mm}$). This equipment is used to display products with temperature class M1 (-1°C to $+5^\circ \text{C}$). It was installed a remote mechanical system with a compressor Octagon 2DC-3.2 and water condenser. The

measuring instruments were selected in order to obtain reliable measurements of the relevant physical properties variation collected every minute during the experimental test. The experimental tests (ET) followed EN ISO 23953 (2005) and were performed in a climatic chamber designed in accordance as shown in Figure 2a. Figure 2b shows the middle section of the ORDC. In DAG, RAG and ambient were placed temperature and humidity sensors Super MT 530. Temperature sensors type PT1000 were placed in the test packages (product simulators). A Coriolis flowmeter MASSFLO 2100 DI 6 was installed at the liquid refrigerant line. Table 1 shows the experimental techniques and probes/experimental measuring devices used to collect the relevant physical properties.

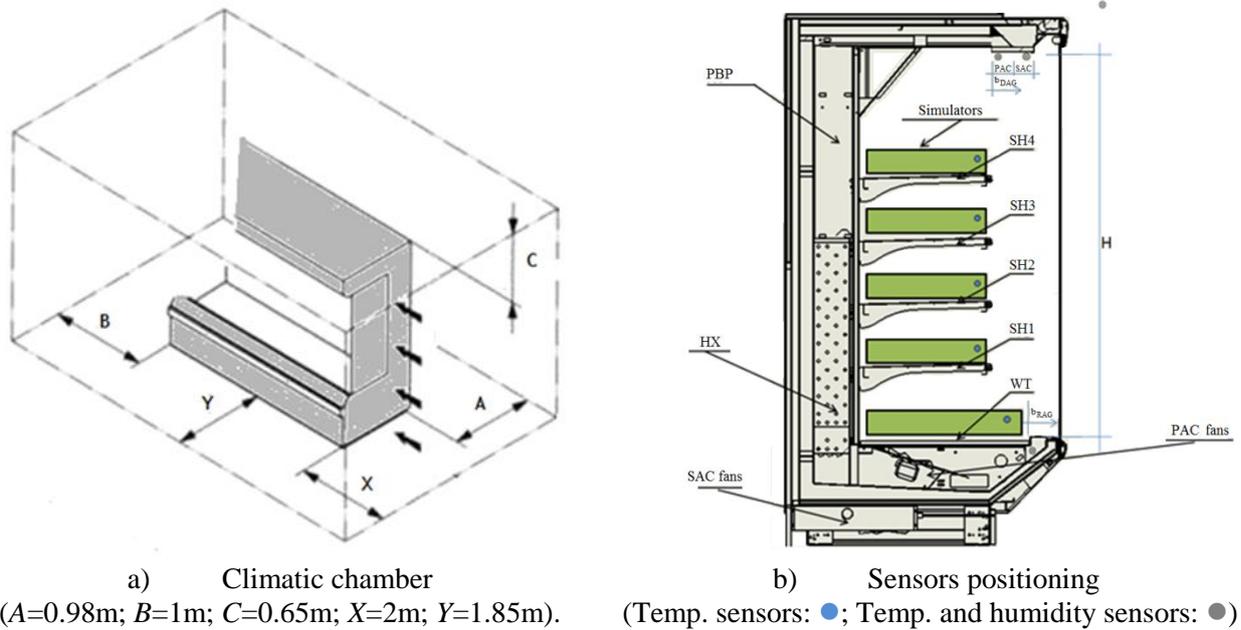


Figure 2. Climatic chamber and sensors location on the ORDC.

Table 1. Experimental techniques and probes/experimental measuring devices.

Experimental technique	Model	Measuring range	Accuracy
Thermometry	PT 1000	-40°C to +80°C	± 0.3 °C
	MT 530 Super	-10°C to 70°C	± 1.5 °C
Hygrometry	MT 530 Super	20% to 85%	± 5%
Anemometry	HTA 4200	0,3 m·s ⁻¹ to 34 m·s ⁻¹	± 1%
Flowmetry	MASSFLO 2100	0 to 1000 kg·h ⁻¹	0.1%
Barometry	AKS 32	0 to 200 psig	± 0.3%

2.2. Experimental testing procedure

Experimental tests (ET) were performed for initial evaluation of the ORDC. As the PBP airflow ratio, β , calculated by eq. (7) considering constant air density., and the characteristic length of DAG influence the *TEF* and overall energy consumption, tests were conducted to four different levels of total air flow, i.e. to four different levels of mass air flow distributed by the DAG_{PAC} and PBP ($\dot{m} = \dot{m}_{PAC} + \dot{m}_{PBP}$). The system control is provided by a frequency inverter connected to the fans of DAG_{PAC}. After identifying the best configuration for the PBP distribution i.e. its porosity, the fans of DAG_{SAC} were also connected. With this procedure, the air curtain thickness was doubled. The air velocity in DAG_{SAC} outlet was modulated to five different levels via control of the frequency inverter connected to the fans of DAG_{SAC}. The PBP was initially closed with tape as shown in Figure 3 for the first four tests (ET1 to ET4). The tapes were partially withdrawn at each series of ET with four levels of fans rotation velocity. The tapes were taken by its numerical order (as shown in Figure 3) to obtain a better distribution of air over the shelves. The procedure consists in firstly to take out all tapes n.º 1, then take out also the tapes with n.º 2, and so on. After identifying the best configuration for β , DAG width was increased from $b_{PAC} = 70$ mm to $b_{PAC+SAC} = 140$ mm for EE17 to EE21.



Figure 3. Open refrigerated display cabinet with perforated back panel completely closed.

The air velocity in DAG (PAC and SAC), RAG and PBP were measured with the propeller type anemometer model HTA4200 in twelve points along the opening perpendicular to flow. These values are shown in Figure 4 in the form of air flow rate for each ET. This figure also includes the value of β for each ET.

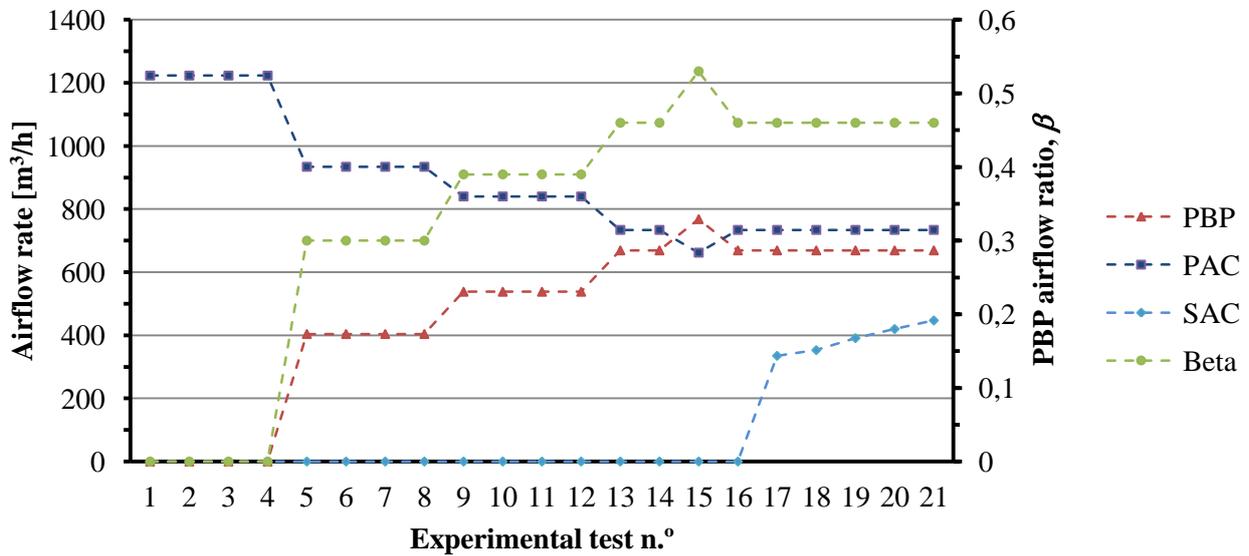


Figure 4. Airflow in PBP, PAC and SAC and PBP airflow ratio.

3. RESULTS ANALYSIS AND DISCUSSION

With the experimental results it was possible to adjust the ORDC and obtain a 10% reduction of energy consumption compared to commercial equipment (given by ET5). The criteria for evaluating the performance of the ORDC was, (1) lowest *TEF*, (2) test packages temperature below 5 °C, and (3) lowest cooling load.

The air temperature and humidity values obtained in the carried out ET (ET1 to ET21) are shown in Figure 5. The test results (EE1 to EE21), showed that: (1) there is an optimal value for β , (2) increasing the DAG thickness reduces TEF and the cooling load. The values of TEF , total cooling load (Q_{tot}) and the average and maximum test packages temperatures (T_{sim}) for the EE are shown in Figure 6. The maximum value of test packages temperature is measured in the well tray for all EE. Q_{tot} values were determined by eq. (1) whereas the TEF values were determined by eq. (5) to eq. (8).

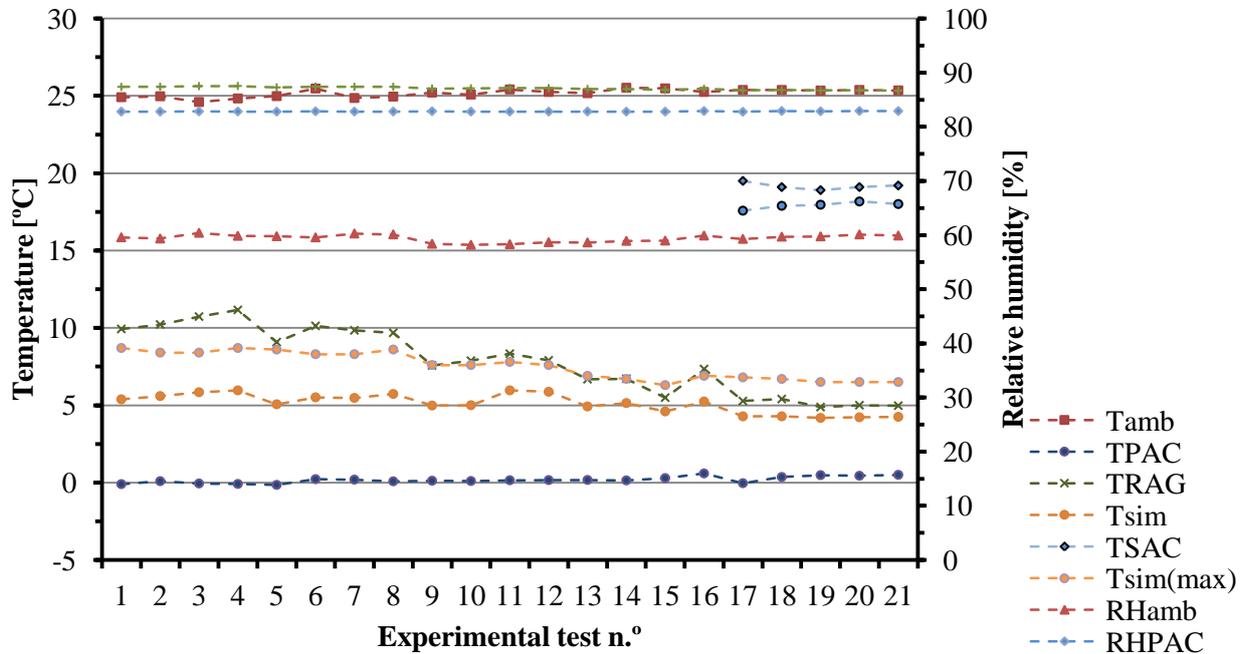


Figure 5. Values of temperature and relative humidity for the experimental tests.

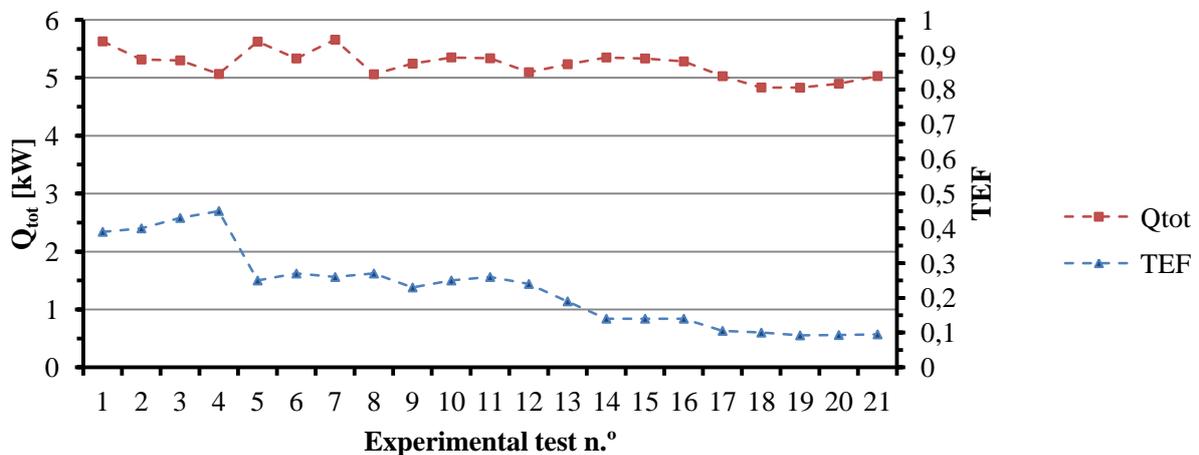


Figure 6. Values of Q_{tot} and TEF for the experimental tests.

In Figure 5, it is possible to see that the air curtain efficiency is a relevant factor to reduce energy consumption and maintenance of product temperature. An efficient sealing ability provided by DAG can be identified by analyzing the TEF values. In order to obtain more efficient equipment considering the previously defined evaluation criteria (lowest TEF , Q_{tot} and T_{sim}), without making major changes in the current design, the best configuration shown in Figure 6 is given by EE19, where $\beta = 0.46$, considering $V_{PAC} = 734 \text{ m}^3\text{h}^{-1}$, $V_{SAC} = 391 \text{ m}^3\text{h}^{-1}$ and $V_{BPB} = 669 \text{ m}^3\text{h}^{-1}$. The mass flows on other ET are different due to the different pressure drop caused in the different configurations.

The air velocity in DAG, RAG e β for each ET is shown in Figure 7. In EE19 was obtained a $u_{DAG} = 0.92 \text{ m s}^{-1}$. Gaspar *et al.* (2011) determined the best performance at $u_{DAG} = 1.5 \text{ m s}^{-1}$, Cao *et al.* (2011) obtained the best performance at $u_{DAG} = 0.8 \text{ m s}^{-1}$ to 1 m s^{-1} , while Yu *et al.* (2009) found an optimum DAG velocity from $u_{DAG} = 0.7 \text{ m s}^{-1}$ to 0.8 m s^{-1} . Comparing the results with these obtained by other authors, we can be stated that the optimal DAG velocity depends on the physical characteristic of the air curtain and the PBP airflow ratio, so for every height/width ratio exists a optimum value for the DAG velocity. With the experimental study, it was possible to adjust this particular ORDC and improve its performance by reducing 10% the energy consumption (ET19) as compared to commercial design (ET15).

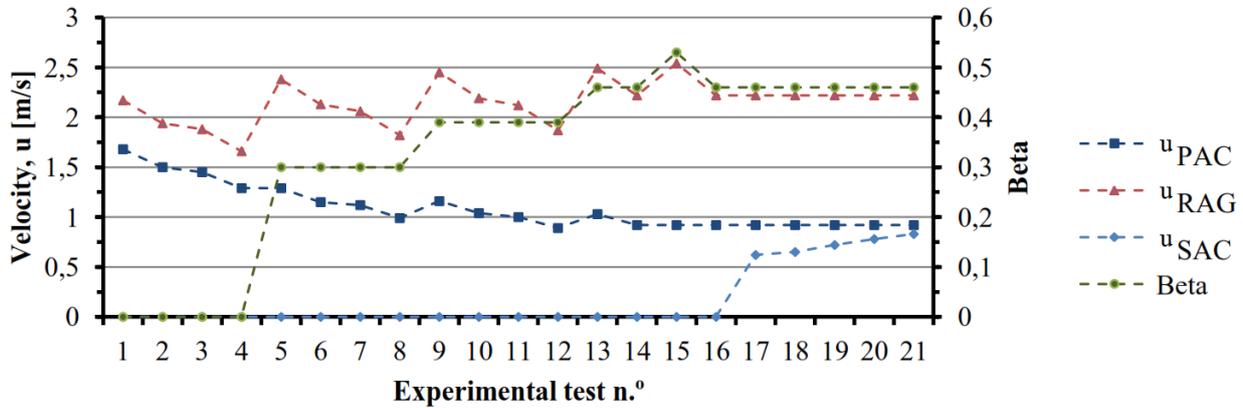


Figure 7. PAC, SAC and RAG velocity and β for the experimental tests in climate class n.º 3 ($T_{amb} = 25 \text{ }^\circ\text{C}$, $RH_{amb} = 60\%$, $u_{amb} = 0.15 \text{ m s}^{-1}$).

4. CONCLUSION

This paper includes an optimization technique for open refrigerated display cabinets. This is a test method of great value to industry, since usually it does not have easily the computational resources or expertise to develop CFD modelling, but it can develop experimental studies measuring the thermo-physical parameters to quantify the air curtain flow. With the experimental results it was possible to identify a value for the airflow rate and its distribution between the PBP and DAG that provides a design with better performance. The optimum values are given by the experimental test where $u_{PAC} = 0.92 \text{ m s}^{-1}$; $u_{SAC} = 0.72 \text{ m s}^{-1}$; $u_{RAG} = 2.22 \text{ m s}^{-1}$; $b_{DAG} = 140 \text{ mm}$; and $\beta = 0.46$. With the development of this work, it is evident the fact that for each type of vertical open refrigerated display cabinet with a height/width ratio different from the model where presented, there are optimum values for β and DAG and RAG velocities.

NOMENCLATURE

b	air curtain width	(m)	Subscripts
g	Gravitational accelerations	(m s^{-1})	amb ambient
Gr	Grashof number	(-)	DAG Discharge air grille
H	Air curtain height	(m)	ET Experimental test
i	enthalpy	(J kg^{-1})	HX Heat exchanger
\dot{m}	Mass flow rate	(kg h^{-1})	IB Insulating body
\dot{Q}	Thermal power	(W)	PAC Primary Air
Re	Reynolds number	(-)	RAG Return air grille
Ri	Richardson number	(-)	SAC Secondary Air
RH	Relative humidity	(%)	Curtain
T	Temperature	(K)	SH Shelve
u	Velocity	(m s^{-1})	sim simulator
V	Airflow rate	(m^3/h)	tot total
X	Dimensionless temperature	(-)	

Abbreviation

CFD Computational fluid Dynamics

DAG	Discharge Air Grille
RAG	Return Air Grille
PBP	Perforated Back Panel
TEF	Thermal Entrainment Factor
PAC	Primary Air Curtain
SAC	Secondary Air Curtain

Greek symbols

θ	Airflow direction	($^{\circ}$)
ν	Kinematic viscosity	(m^2s^{-1})
ξ	Thermal expansion coefficient	(K^{-1})
β	Back panel airflow ratio	(-)

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